

## Production of $\alpha$ -arbutin from Hydroquinone by *Bacillus subtilis* TISTR 1248 and *Xanthomonas campestris* TISTR 2065

Aurasorn Saraphanchotiwitthaya<sup>1,2\*</sup>, and Pattana Sripalakit<sup>2,3</sup>

<sup>1</sup>Department of Pharmaceutical Technology, Faculty of Pharmaceutical Sciences, Naresuan University, Phitsanulok 65000, Thailand

<sup>2</sup>Pharmaceutical Biotechnology Research Unit, Faculty of Pharmaceutical Sciences, Naresuan University, Phitsanulok 65000, Thailand

<sup>3</sup>Department of Pharmaceutical Chemistry and Pharmacognosy, Faculty of Pharmaceutical Sciences, Naresuan University, Phitsanulok 65000, Thailand

\*Corresponding author. E-mail: aurasorns@nu.ac.th  
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### ABSTRACT

*$\alpha$ -Arbutin has been used in the cosmetic industry as a skin-whitening agent and in pharmaceutical applications. It can be synthesised by a chemical reaction and a microbial enzyme. This investigation aims to study the production of  $\alpha$ -arbutin by microbial fermentation, using whole cells of *Bacillus subtilis* TISTR 1248 or *Xanthomonas campestris* TISTR 2065 as a biocatalyst for the transglucosylation reaction between hydroquinone and disaccharide (sucrose and maltose). The amount of  $\alpha$ -arbutin in the biotransformation medium under different concentrations of hydroquinone, disaccharides and ascorbic acid was analysed by a high-performance liquid chromatography (HPLC) technique. The results showed that *X. campestris* TISTR 2065 was more effective than *B. subtilis* TISTR 1248 on  $\alpha$ -arbutin production. The production yield obtained from using sucrose or maltose as a donor was not statistically different. The addition of ascorbic acid resulted in a slight increase in  $\alpha$ -arbutin production, spending less time to reach the maximum yield. The maximum production of  $\alpha$ -arbutin of approximately  $366.33 \pm 21.13$  mg/l (day 12) was achieved from the biotransformation medium containing 5%w/v hydroquinone and 3%w/v sucrose together with 0.2 mM ascorbic acid by *X. campestris* TISTR 2065. The elucidation of the  $\alpha$ -arbutin structure and the biological activity of the biotransformation mixture containing  $\alpha$ -arbutin needs further investigation.*

**Keywords:**  $\alpha$ -Arbutin, Hydroquinone, *Bacillus subtilis* TISTR 1248, *Xanthomonas campestris* TISTR 2065

## INTRODUCTION

$\alpha$ - and  $\beta$ -arbutin are glycosylated hydroquinones that have been used in phytotherapy and the cosmetic industry (Kwiecień et al., 2013). Arbutin has been used for the treatment of urinary tract infection, kidney stones and diuresis (Seo et al., 2012a). The *in vivo* antitussive activity of arbutin from plants was reported (Strapková et al., 1991). Moreover, the anti-inflammatory effects of arbutin in lipopolysaccharide-stimulated BV2 microglial cells has been shown (Lee et al., 2012). Its antifungal and antioxidant activities have also been proven (Azadbakht et al., 2004). In cosmetics, both the compounds exhibited inhibitory activity on tyrosinase, an enzyme involved in melanin synthesis (Akiu et al., 1988); this enzyme catalyses the hydroxylation of tyrosine to 3-(3, 4-dihydroxyphenyl)-alanine (DOPA) and the oxidation of DOPA to dopaquinone (Sugimoto et al., 2005). Therefore,  $\alpha$ - and  $\beta$ -arbutin has been widely used as skin whitening agents (Akiu et al., 1988; Seo et al., 2012b); however, the whitening effect of  $\alpha$ -arbutin was more than ten times higher than  $\beta$ -arbutin (Sugimoto et al., 2003). The half maximum inhibitory concentration ( $IC_{50}$ ) of  $\alpha$ -arbutin on human tyrosinase was 2.0 mM which was more potent than natural arbutin at a concentration higher than 30 mM (Sugimoto et al., 2003; Sugimoto et al., 2007). Recently, the demand for  $\alpha$ -arbutin has increased significantly in many parts of the world (Liu et al., 2013).  $\beta$ -arbutin can be extracted from various plant species including bearberry, wheat and pear (Liu et al., 2013), it can be produced via the biotransformation of hydroquinone in *in vitro* cultures of numerous plant species (Seo et al., 2012a).  $\alpha$ -Arbutin is mainly produced via microbial biotransformation by using whole cells and carbohydrate-active enzymes (Liu et al., 2013). From previous studies, *Bacillus subtilis* X-23 was reported as an effective strain among 600 microbial strains screened from soil for  $\alpha$ -arbutin production by glycosylation of hydroquinone and possessed  $\alpha$ -amylase activity. Using hydroquinone as a glycosyl acceptor and maltopentaose as the donor reached an  $\alpha$ -arbutin production yield of 32.4% (Nishimura et al., 1994). When using *Xanthomonas campestris* WU-9701 cells as biocatalysts and maltose as a glucosyl donor for  $\alpha$ -arbutin production, a maximum molar conversion yield of 93% was obtained (Kurosu et al., 2002). Mutant *Xanthomonas maltophilia* BT-112 was screened using various mutation techniques. Under optimised conditions, the maximum  $\alpha$ -arbutin yield of 30.6 g/l (93.6%) was obtained from 120 mM hydroquinone (Liu et al., 2013).

In this study, we aimed to investigate the efficiency of two culture collections, *Bacillus subtilis* TISTR 1248 and *Xanthomonas campestris* TISTR

2065, from the Thailand Institute of Scientific and Technological Research (TISTR) on the production of  $\alpha$ -arbutin. Various concentrations of substrates and additives were optimised.

## MATERIAL AND METHODS

### Strains and chemicals

*Bacillus subtilis* TISTR 1248 and *Xanthomonas campestris* TISTR 2065 were purchased from the Thailand Institute of Scientific and Technological Research (Pathum Thani, Thailand).  $\alpha$ -arbutin standards were purchased from the Sigma–Aldrich Chemical Co. (St. Louis, Mo, USA), sucrose and maltose were purchased from Merck (Germany), peptones and yeast extract were purchased from the HiMedia Laboratories (India), and the other reagents were of an analytical grade and purchased from Merck (Germany).

### Preparation of medium and stock cell suspensions

The medium for the cell growth and biotransformation contained 20 g/l of sucrose, 10 g/l of peptone, 0.5 g/l of  $\text{MgSO}_4$ , 1 g/l of  $\text{K}_2\text{HPO}_4$ , 1 g/l of  $\text{KH}_2\text{PO}_4$ , 2 g/l of NaCl and 1 g/l of  $\text{NaHCO}_3$  in distilled water; the pH was adjusted to 7.0 prior to sterilisation at 121 °C for 20 min. Stock cell suspensions were prepared by adding a loopful of inoculum from the slant (nutrient agar: 5 g/l of peptic digest of animal tissue, 5 g/l of NaCl, 1.5 g/l of beef extract, 1.5 g/l of yeast extract and 15 g/l of agar) into the medium and cultured under shaking conditions at  $25 \pm 2$  °C, 220 rpm (revolutions per minute) for 48 h on an orbital shaker (SK3PO, CT laboratory, USA).

### Effect of hydroquinone (HQ) concentrations

A sterile biotransformation medium with an initial volume of 45 ml in 250 ml Erlenmeyer flasks was inoculated with 5 ml stock cell suspensions of *B. subtilis* TISTR 1248 or *X. campestris* TISTR 2065. Hydroquinone concentrations at 1, 3 and 5% w/v were added into the biotransformation medium and cultured under conditions at  $25 \pm 2$  °C, 220 rpm for 18 days on an orbital shaker. During the biotransformation process, 1.5 ml of the culture medium was collected at 0, 7, 9, 12, 15 and 18 days for the  $\alpha$ -arbutin analysis. The microbial strain with an appropriate HQ concentration which gave the maximum yield of  $\alpha$ -arbutin was selected for further experiment.

### Effect of carbon sources

Five ml of *X. campestris* TISTR 2065 cell suspension was added into a 45 ml sterile medium contained 5% w/v HQ and 1, 2 and 3% w/v sucrose or maltose in 250 ml Erlenmeyer flasks. The biotransformation medium was cultured at 25

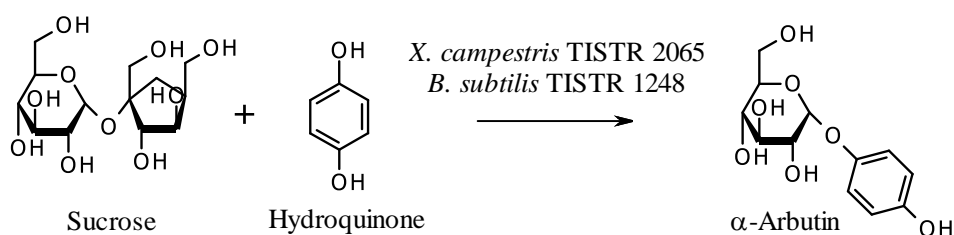
$\pm 2\text{ }^{\circ}\text{C}$ , 220 rpm for 18 days. The culture medium was collected at 0, 7, 9, 12, 15 and 18 days to analyse  $\alpha$ -arbutin. All the experiments were conducted in triplicate.

### Effect of ascorbic acid

Five ml of *X. campestris* TISTR 2065 cell suspension was added into 45 ml of sterile medium containing 5% w/v HQ and 3% w/v sucrose or maltose in 250 ml Erlenmeyer flasks. Various concentrations of ascorbic acid at 0.1, 0.2 and 0.3 mM were added into each flask and cultured under the same conditions. The culture medium was collected at 0, 7, 9, 12, 15 and 18 days to analyse  $\alpha$ -arbutin. All the experiments were conducted in triplicate.

### HPLC analysis

$\alpha$ -Arbutin was detected using high-performance liquid chromatography (HPLC) (Shimadzu Corporation, Japan) under the following conditions: column, C18 Lunar<sup>TM</sup> column (250 mm  $\times$  4.60 mm, 5  $\mu\text{m}$ ; Phenomenex, CA, USA); temperature,  $25 \pm 2\text{ }^{\circ}\text{C}$ ; mobile phase, methanol–water (5:95, v/v) with 0.1% acetic acid v/v; flow rate, 1.0 ml/min; ultraviolet detector, wavelength 280 nm. The calibration curve of  $\alpha$ -arbutin standard solution at concentrations between 0.5–10.0 g/l showed good linearity. The regression line for  $\alpha$ -arbutin was  $y = 18.128x - 0.2697$  ( $R^2 = 0.9997$ ), where  $y$  is the peak area ( $\times 10^{-6}$ ) and  $x$  is concentration of  $\alpha$ -arbutin (g/l). Microbial biotransformation reaction to produce  $\alpha$ -arbutin from hydroquinone, and their chemical structures are shown in Figure 1.



**Figure 1.** Microbial biotransformation of hydroquinone to  $\alpha$ -arbutin

## RESULTS

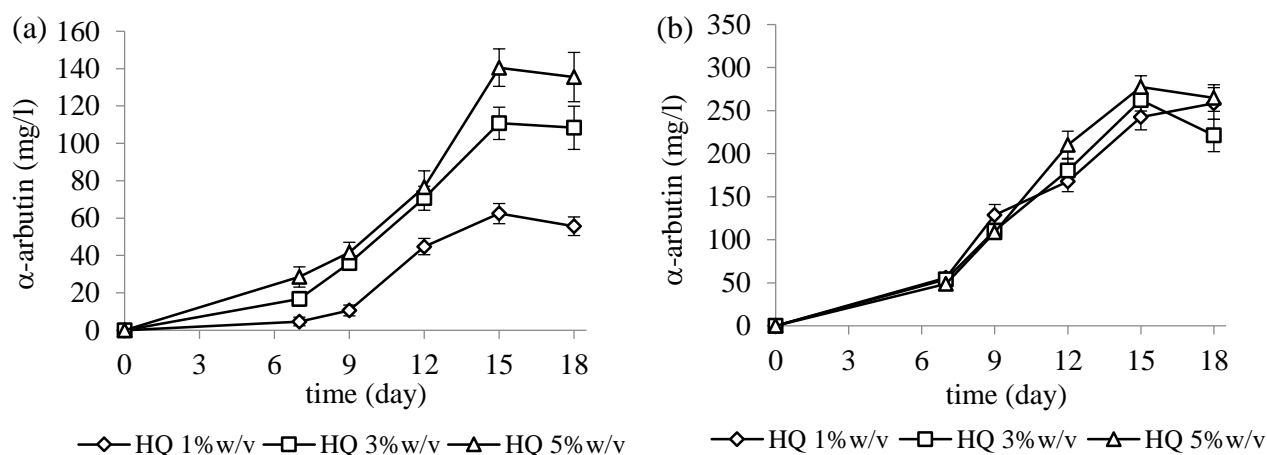
### Effects of hydroquinone concentrations

*B. subtilis* TISTR 1248 and *X. campestris* TISTR 2065 were used to produce  $\alpha$ -arbutin in this study. The effect of different concentrations of hydroquinone in the culture medium was investigated, and the results are shown

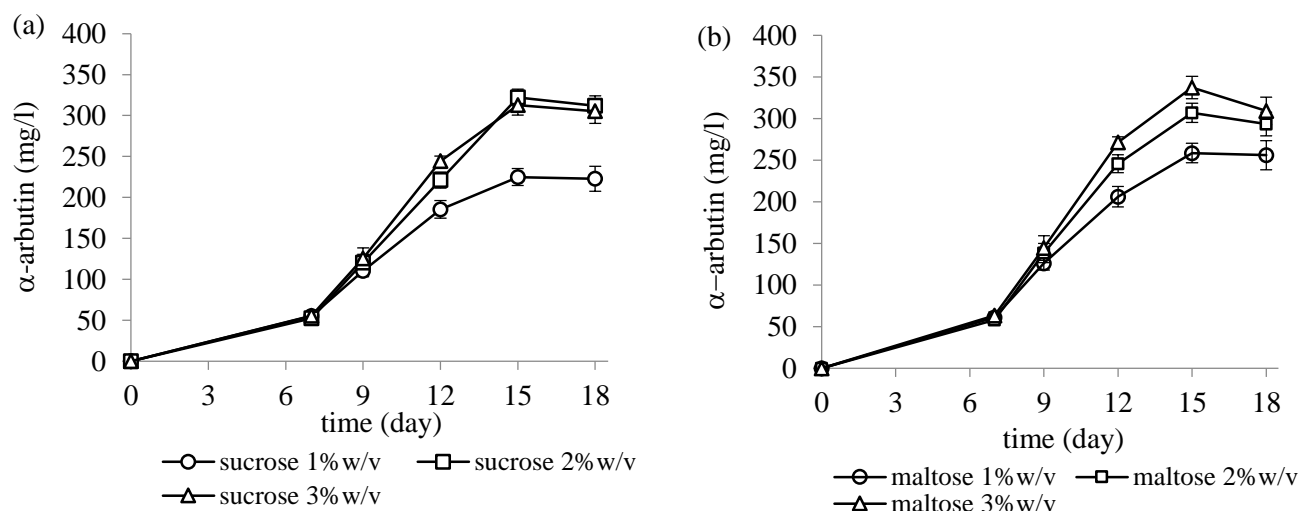
in Figure 2. The results showed that both *B. subtilis* TISTR 1248 and *X. campestris* TISTR 2065 can produce  $\alpha$ -arbutin. For both strains, using hydroquinone at a high concentration in the culture medium resulted in a higher yield of  $\alpha$ -arbutin. In the presence of 5% w/v hydroquinone, *X. campestris* TISTR 2065 produced the maximum yield of  $\alpha$ -arbutin of approximately  $277.66 \pm 12.72$  mg/l at day 15 which was more than that produced by *B. subtilis* TISTR 1248 ( $140.52 \pm 10.06$  mg/l at day 15). Therefore, *X. campestris* TISTR 2065 was selected for further study.

### Effects of carbon sources

The effect of two carbon sources, sucrose and maltose, at different concentrations for  $\alpha$ -arbutin production by *X. campestris* TISTR 2065 were studied, the results are shown in Figure 3. *X. campestris* TISTR 2065 can produce  $\alpha$ -arbutin from both sucrose and maltose at all the tested concentrations. A higher yield of  $\alpha$ -arbutin was produced from using a high concentration of sucrose and maltose. The maximum yield of  $\alpha$ -arbutin was obtained from using 5% w/v hydroquinone and 3% w/v maltose. However, the production yield of  $\alpha$ -arbutin obtained using 2 and 3% w/v sucrose or maltose as a donor was not statistically different.



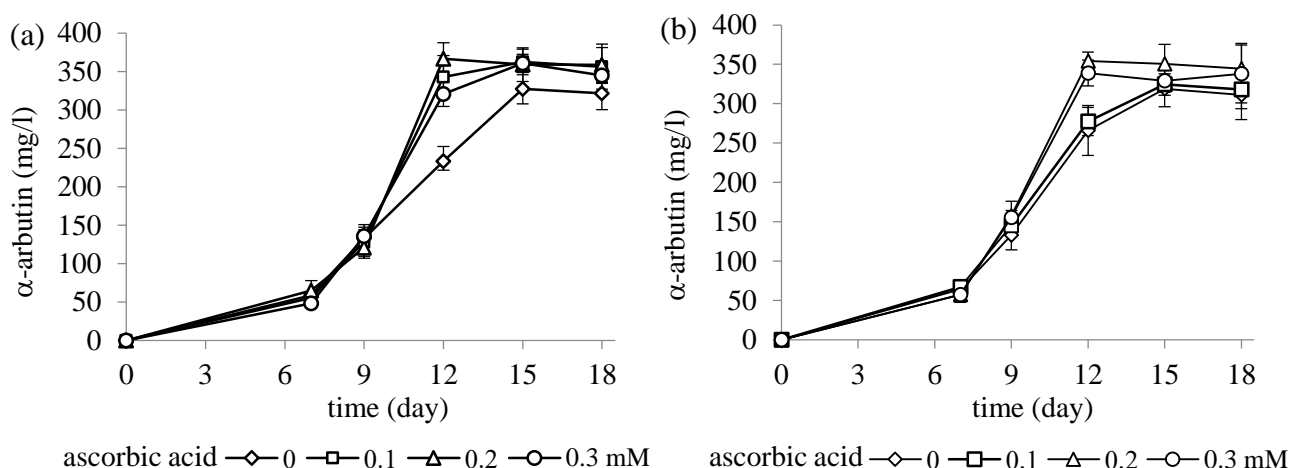
**Figure 2.** The effect of hydroquinone (HQ) at different concentrations on  $\alpha$ -arbutin production by (a) *Bacillus subtilis* TISTR 1248 and (b) *Xanthomonas campestris* TISTR 2065. The results are represented as the mean  $\pm$  SE (n = 3).



**Figure 3.** The effect of carbon sources; (a) sucrose and (b) maltose at different concentrations on  $\alpha$ -arbutin production by *Xanthomonas campestris* TISTR 2065. The results are represented as the mean  $\pm$  SE (n = 3).

### Effects of ascorbic acid

The influence of ascorbic acid at different concentrations in the culture medium of *X. campestris* TISTR 2065 for  $\alpha$ -arbutin production from 5%w/v hydroquinone and 3%w/v sucrose or maltose was studied. As shown in Figure 4, the addition of ascorbic acid resulted in a slight increment of  $\alpha$ -arbutin production reaching a maximum yield in less production time. The maximum yield of  $\alpha$ -arbutin of approximately  $366.33 \pm 21.13$  mg/l (day 12) was obtained from using 5%w/v HQ and 3%w/v sucrose with the addition of 0.2mM ascorbic acid; however, there was no statistical difference in the  $\alpha$ -arbutin yield among the different doses of ascorbic acid in both in sucrose and maltose.



**Figure 4.** The effect of ascorbic acid at different concentrations on  $\alpha$ -arbutin production from 5%w/v hydroquinone and (a) 3%w/v sucrose and (b) 3%w/v maltose by *Xanthomonas campestris* TISTR 2065. The results are represented as the mean  $\pm$  SE (n = 3).

## DISCUSSION

$\alpha$ -Arbutin is a glycosylated hydroquinone that is mainly used as a powerful skin whitening agent in the cosmetic industry. These compounds can be produced using chemical synthesis, but microbial bioconversion is preferred due to its specificity and eco-friendly environments (Zhu et al., 2018). There have been many previous investigations on the production of  $\alpha$ -arbutin using whole cells and microbial enzymes. Whole cells such as *B. subtilis* X-23 (Nishimura et al., 1994), *X. campestris* Wu-9701 (Kurosu et al., 2002), *X. maltophilia* BT-112 (Liu et al., 2014) and microbial enzymes such as  $\alpha$ -glucosidase from *X. campestris* WU-9701 (Sato et al., 2012), dextranucrase from *Leuconostoc mesenteroides* (Seo et al., 2009) and amylosucrase from *Deinococcus geothermali*s (Park et al., 2011; Seo et al., 2012b) were used in the studies.

The percentage yield of  $\alpha$ -arbutin production obtained from the enzymatic and microbial bioconversion of hydroquinone varied from 0.4 to 93.6%. The highest yield of  $\alpha$ -arbutin (30.6 g/l) was obtained using mutant *X. maltophilia* BT-112 cell with 120 mM HQ and 20 g/l of sucrose (Liu et al., 2013). Moreover,  $\alpha$ -arbutin was effectively produced using lyophilised *X. campestris* WU-9701 cells with 45 mM HQ and 1.2 M maltose, reaching the highest  $\alpha$ -arbutin yield of 11.4 g/l (Kurosu et al., 2002).

Based on the previous researches, we investigated the production of  $\alpha$ -arbutin using two related microbial strains from the TISTR collection including *B. subtilis* TISTR 1248 and *X. campestris* TISTR 2065. It has been found that *X. campestris* TISTR 2065 was more effective than *B. subtilis* TISTR 1248 in  $\alpha$ -arbutin production. HQ at a high concentration (5% w/v or 454 mM) resulted in a higher production of  $\alpha$ -arbutin. A previous study reported that cells undergo apoptosis when using a high concentration of HQ in the medium (Liu et al., 2013); however, this study indicated that *X. campestris* TISTR 2065 tolerated a high concentration of HQ.

For  $\alpha$ -arbutin production, carbon sources are necessary nutrients for microbial cell growth and act as a glucosyl donor. A previous study performed by Liu et al. (2013) found that among various carbon sources, sucrose and maltose were suitable for cell growth and  $\alpha$ -arbutin production by mutant *Xanthomonas maltophilia* BT-112. Based on these findings, sucrose and maltose were applied as carbon sources in our study. We found that *X. campestris* TISTR 2065 can employ both sucrose and maltose as a substrate to produce  $\alpha$ -arbutin and different concentrations of these disaccharides affected the production yield of  $\alpha$ -arbutin. Although, using maltose provided an  $\alpha$ -arbutin yield higher than sucrose; however, sucrose was cheaper than maltose resulted in a more cost-effective production.

Liu et al. (2013) suggested an appropriate ratio of sucrose to HQ at 2:1 (mol) for effective  $\alpha$ -arbutin production. This ratio was different from our study which was 0.20:1 (mol). The different sucrose to HQ ratio might be appropriate for different strains, leading to their efficiency in the biotransformation process.

Seo et al. (2012a) reported that using ascorbic acid can improve the production yield of  $\alpha$ -arbutin. In the absence of ascorbic acid, the production yield of  $\alpha$ -arbutin was significantly low (1.3%), in the presence of 0.2 mM ascorbic acid, a maximum conversion yield of  $\alpha$ -arbutin of more than 90% was obtained. In our study, the addition of ascorbic acid in the biotransformation medium containing 5%w/v hydroquinone and sugar (3%w/v sucrose or maltose) for  $\alpha$ -arbutin production by *X. campestris* TISTR 2065 was not in accordance with this previous investigation. We observed a slight increase in the  $\alpha$ -arbutin yield, requiring less time to reach the maximum yield. Ascorbic acid, acting as an antioxidant, may increase the stability of hydroquinone in the mixture, resulting in the effective production of  $\alpha$ -arbutin. However, the efficiency of the reactive enzymes and the microbial strain itself remained a significant limitation. The optimization of fermentation conditions might be further investigated to increase the glycosylation activity of wild-type strain.

Recently, whole-cell biocatalysis using engineered *E. coli* together with batch-feeding strategy have been used to increase arbutin production. *E. coli* cells containing overexpressed amylosucrase, a sucrose-utilizing glycosidase enzyme isolated from *X. campestris* pv. *campestris* 8004, were used to catalyze glycosylation of hydroquinone. The batch-feeding whole-cell biocatalysis by amylosucrase was designed to eliminate hydroquinone inhibition, resulting enhanced yield (306 mM) and molar conversion rate (95%) (Zhu et al., 2019a). Process scale-up of these system was evaluated in 5000-L reactor, producing the highest yields (398 mM per 4000-l reaction volume) and productivities (4.5–4.9 kg kl<sup>-1</sup> h<sup>-1</sup>) which can be successfully applied for industrial production of  $\alpha$ -arbutin (Zhu et al., 2019b). For our further investigations, a fed-batch strategy and engineered *E. coli* containing enzyme might be determined to enhance arbutin production.

## CONCLUSION

At present, skin-lightening agents are substantially attractive for both pharmaceutical and cosmeceutical approaches, as a response to the rising demand for treatments of the disorders of skin pigmentations. Therefore, natural arbutin which was synthesised by two wild type microbial strains, *X. campestris* TISTR 2065 and *B. subtilis* TISTR 1248, was investigated in this study. We concluded that *X. campestris* TISTR 2065 was more effective than *B. subtilis* TISTR 1248 for  $\alpha$ -arbutin production. Both sucrose and maltose can be used as carbon sources



for cells growth and acted as a glucosyl donor. The maximum yield of  $\alpha$ -arbutin ( $366.33 \pm 21.13$  mg/l) was achieved from the biotransformation medium consisting of 5%w/v hydroquinone and 3%w/v sucrose with 0.2 mM ascorbic acid (pH 7.0) by *X. campestris* TISTR 2065 under conditions of  $25 \pm 2$  °C, 220 rpm. The elucidation of the  $\alpha$ -arbutin structure and the biological activity of the biotransformation mixture containing  $\alpha$ -arbutin needs further investigation. In the future, genetic recombination technology needs to be applied to enhance the expression of  $\alpha$ -arbutin-producing enzymes to increase  $\alpha$ -arbutin production.

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